



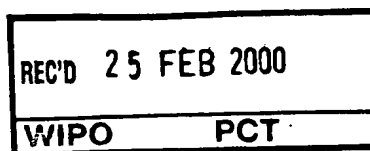
The
Patent
Office

PCT/GB 04/700128
19 JANUARY 2000

INVESTOR IN PEOPLE

GB00/00123

**PRIORITY
DOCUMENT**
SUBMITTED OR TRANSMITTED IN
COMPLIANCE WITH RULE 17.1(a) OR (b)



The Patent Office
Concept House
Cardiff Road
Newport
South Wales
NP10 8QQ

I, the undersigned, being an officer duly authorised in accordance with Section 74(1) and (4) of the Deregulation & Contracting Out Act 1994, to sign and issue certificates on behalf of the Comptroller-General, hereby certify that annexed hereto is a true copy of the documents as originally filed in connection with the patent application identified therein.

In accordance with the Patents (Companies Re-registration) Rules 1982, if a company named in this certificate and any accompanying documents has re-registered under the Companies Act 1980 with the same name as that with which it was registered immediately before re-registration save for the substitution as, or inclusion as, the last part of the name of the words "public limited company" or their equivalents in Welsh, references to the name of the company in this certificate and any accompanying documents shall be treated as references to the name with which it is so re-registered.

In accordance with the rules, the words "public limited company" may be replaced by p.l.c., plc, P.L.C. or PLC.

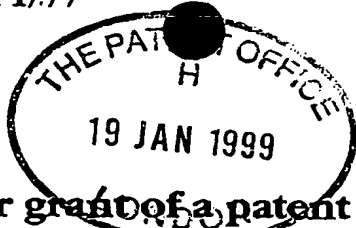
Re-registration under the Companies Act does not constitute a new legal entity but merely subjects the company to certain additional company law rules.

Signed

Andrew Gersey

Dated 2 February 2000

THIS PAGE BLANK (USPTO)



20 JAN 99 E419055-1 C03018
P01/7700 0.00 - 9901139.7

Request for grant of a patent

(See the notes on the back of this form. You can also get an explanatory leaflet from the Patent Office to help you fill in this form.)

The Patent Office

Cardiff Road
Newport
Gwent NP9 1RH

1. Your reference

MGH/MG/P08813GB

2. Patent application number

(The Patent Office will fill in this part)

9901139.7

19 JAN 1999

3. Full name, address and postcode of the or of each applicant (underline all surnames)

COMMON SERVICES AGENCY
TRINITY PARK HOUSE
SOUTH TRINITY ROAD
EDINBURGH EH5 3SE

Patents ADP number (if you know it)

If the applicant is a corporate body, give the country/state of its incorporation

606497001

4. Title of the invention

TREATMENT OF PROTEIN-CONTAINING LIQUIDS

5. Name of your agent (if you have one)

"Address for service" in the United Kingdom to which all correspondence should be sent (including the postcode)

CRUIKSHANK & FAIRWEATHER
19 ROYAL EXCHANGE SQUARE
GLASGOW G1 3AE

Patents ADP number (if you know it)

547002

6. If you are declaring priority from one or more earlier patent applications, give the country and the date of filing of the or of each of these earlier applications and (if you know it) the or each application number

Country

Priority application number
(if you know it)

Date of filing
(day / month / year)

7. If this application is divided or otherwise derived from an earlier UK application, give the number and the filing date of the earlier application

Number of earlier application

Date of filing
(day / month / year)

8. Is a statement of inventorship and of right to grant of a patent required in support of this request? (Answer 'Yes' if:

- a) any applicant named in part 3 is not an inventor, or
 - b) there is an inventor who is not named as an applicant, or
 - c) any named applicant is a corporate body.
- See note (d))

Patents Form 1/77

9. Enter the number of sheets for any of the following items you are filing with this form. Do not count copies of the same document

Continuation sheets of this form

Description	13	CA.
Claim(s)	1	
Abstract	-	
Drawing(s)	-	

10. If you are also filing any of the following, state how many against each item.

Priority documents	
Translations of priority documents	
Statement of inventorship and right to grant of a patent (Patents Form 7/77)	
Request for preliminary examination and search (Patents Form 9/77)	
Request for substantive examination (Patents Form 10/77)	
Any other documents (please specify)	

11. I/We request the grant of a patent on the basis of this application.

Signature CRIKSHANK & FAIRWEATHER Date 14/1/99

12. Name and daytime telephone number of person to contact in the United Kingdom CRIKSHANK & FAIRWEATHER 19/01/99
Dr. M.G. Horner - 0141-221-5767

Warning

After an application for a patent has been filed, the Comptroller of the Patent Office will consider whether publication or communication of the invention should be prohibited or restricted under Section 22 of the Patents Act 1977. You will be informed if it is necessary to prohibit or restrict your invention in this way. Furthermore, if you live in the United Kingdom, Section 23 of the Patents Act 1977 stops you from applying for a patent abroad without first getting written permission from the Patent Office unless an application has been filed at least 6 weeks beforehand in the United Kingdom for a patent for the same invention and either no direction prohibiting publication or communication has been given, or any such direction has been revoked.

Notes

- If you need help to fill in this form or you have any questions, please contact the Patent Office on 0645 500505.
- Write your answers in capital letters using black ink or you may type them.
- If there is not enough space for all the relevant details on any part of this form, please continue on a separate sheet of paper and write "see continuation sheet" in the relevant part(s). Any continuation sheet should be attached to this form.
- If you have answered 'Yes' Patents Form 7/77 will need to be filed.
- Once you have filled in the form you must remember to sign and date it.
- For details of the fee and ways to pay please contact the Patent Office.

TREATMENT OF PROTEIN-CONTAINING LIQUIDS

The present invention relates to a method for the removal of abnormal infective prion proteins associated with transmissible spongiform encephalopathies (TSEs) from an aqueous liquid containing biologically active proteins.

The invention also relates to proteins (including foodstuffs and biologically active proteins) and medicinal compositions therefrom where the infective prion has been removed or inactivated.

There is concern about the potential transmission of TSEs such as Creutzfeldt-Jakob Disease (CJD) via whole blood or blood derived biopharmaceuticals. This concern has been heightened by a postulated link between bovine spongiform encephalopathy (BSE) and a new variant form of CJD (vCJD) in humans. CJD is a progressive neurodegenerative disease caused by an unusual infectious agent that replicates in the lymphoreticular tissue and the central nervous system of its host. The nature of the agent is unresolved at present but two main hypotheses have been advanced. The first is the prion or infectious protein hypothesis; and the second is the virion hypothesis which encompasses a combination of host encoded protein with regulatory nucleic acid.

Medicinal compositions for intravenous infusion, intramuscular infusion and topical application have been prepared from human blood plasma for over four decades in a specialised but significant section of the pharmaceutical processing industry. A principal area of concern in the

safety of these products has been potential contamination with blood born viruses. However, the development of screening methods together with technology for the inactivation or removal of potentially contaminating viruses has greatly improved the safety of blood and preparations derived therefrom.

There is currently considerable concern about the possibility that biopharmaceutical products from human or animal sources may transmit TSEs. Although the precise nature of the infective agent in TSEs is at present unclear, TSEs such as Scrapie in sheep and CJD or vCJD in humans are associated with abnormal prion related proteins (PrPs). Suitable screening methods have not yet been developed for abnormal PrPs, which are also extremely resistant to physical and chemical means of inactivation. For example, the EEC regulatory document (CPM Guidelines for Minimising the Risk of Transmitting Agents causing Spongiform Encephalopathies by Medicinal Products: Biologicals, 20, pp155-158, 1992) recommends autoclaving at about 130°C for up to an hour, treatment with 1N sodium hydroxide for 1 hour or treatment with sodium hypochlorite for 1 hour. Such techniques are, however, quite unsuitable for the treatment of biologically active protein - containing materials since they result in total inactivation of the protein.

There is therefore a need to develop methods of removal or inactivation of abnormal infective prion proteins from animal, or human derived medicinal or food products which

are effective yet do not substantially degrade and/or remove the biological activity or food value of the product.

A major problem relates to the ill defined nature of the abnormal prion protein. The normal form of this protein is found in mammalian cells and is present in high levels in brain and lymphoreticular tissues. It is composed of highly membrane associated 33-35KDa phosphoinositol glycoprotein, which is completely sensitive to digestion with proteinase K. The infectious form of the protein has been shown to exist in an altered conformational form, and contains a high level of β pleated-sheet. The change in conformation is thought to result in the protein becoming highly insoluble, forming aggregates which then deposit in the infected tissue as fibrils or amyloid plaques. The unknown properties of the abnormal prion proteins, and particularly the state of aggregation makes the prediction of suitable removal or inactivation techniques very difficult.

In the prior art, removal or inactivation by chromatographic techniques has been attempted. Hunter and Wilson (J. Gen. Microbiol., 1964, vol. 37 pp251-258) showed examples of the chromatographic behaviour of scrapie-infected brain homogenate on DEAE cellulose adsorption and calcium phosphate columns. International patent application W097/3454 relates to the removal of abnormal prion proteins from solutions of albumin or reagent grade animal serum using typically expensive mixed ion exchange

and hydrophobic solid phases.

Blum et al (BioPharm. 11(4) pp28-34, 1998) investigated the effectiveness of various steps (i.e. heating, precipitation, absorption with filter aid and ion-exchange chromatography) in the production of aprotinin and bovine serum albumin in removing added spikes of scrapie as a model source of TSE. However, it is unclear which of the above elements are essential or required in the removal of the scrapie agent.

Patent specification EP0798003 discloses filtration as a way of removing unwanted contaminants. A positively charged depth filter of 0.25 to 2.0 micron pore size also carrying a cation resin, was used for the removal of viruses from biologically active protein solutions. Morgenthaler (TSE issues, Cambridge Health Tech. Institute CHI, November, 1998, Lisbon, Portugal) has shown that filtration steps (including nanofiltration) can substantially remove added TSE spikes in the fractionation of human plasma.

It is an object of the present invention to further develop and characterise the removal of abnormal infective prion proteins from protein-containing liquids, particularly those derived from human plasma, without unacceptable effects on the nature or biological activity of the proteins.

It is a further object of the present invention to provide a depth filter which can be a single use filter and may be disposed of having removed the abnormal prion

proteins from the process stream.

The invention is based on the surprising discovery that filtration using a depth filter comprising particles having a pore size less than two microns is surprisingly effective in removing abnormal infective prion proteins.

In particular, the invention provides a method for the removal of abnormal infective prion proteins associated with transmissible spongiform encephalopies (TSEs) from an aqueous liquid containing a protein (especially a biologically active protein), which comprises passing the liquid through a depth filter formed of a matrix comprising solid particles of porous material having a pore size less than $2\mu\text{m}$. Typically the filter may be a single use disposable filter.

By the term "removal" is meant the actual removal or inactivation of the abnormal infective prion protein. For practical purposes, the biological activity of an active protein should be substantially maintained at least to a level in excess of 50%, preferably 80%, more preferably 90%.

Removal may be achieved to an extent of at least 10^3 , preferably 10^4 , more particularly 10^5 .

The invention also relates to the treated liquid.

Of particular importance to the fractionation of blood plasma products, is the discovery that filtration may be effectively carried out under non-denaturing conditions for the biologically active protein, and under conditions which do not reduce the solubility of the product protein. In

addition filtration with or without filter aid can be used to remove suspended solids.

The method may be carried out at a pH in the range 4-10, preferably 5-9, and especially 6-8.

The application of heat is unnecessary and the process can be conducted at substantially room temperature or below, in particular in the range -5 to +20°C.

Preferably, the liquid is free of cationic or anionic charged material which may contribute to the reduction of biological activity of the biologically active protein, and in particular may cause activation of sensitive blood coagulation factors. The process is in particular applicable to the treatment of liquids containing albumin, immunoglobulins, Factor IX, thrombin, fibrinogen, Factor VIII and Factor II, IX and X derived from plasma. In addition, the invention is applicable to the treatment of other natural products including foods, drinks, cosmetics etc. It is also applicable to other non-plasma animal-derived products, such as heparin and hormones.

The depth filter generally comprises a binder, such as cellulose, together with a solid porous particulate material such as Kieselguhr, perlite or diatomaceous earth.

The depth filter generally has a thickness in the region 1-10mm, particularly 2-5mm. The material used for the depth filter should have no effect on the protein concerned.

Embodiments of the present invention will now be described by way of example only.

METHODOLOGY

1) Preparation of hamster scrapie spike

Hamster adapted scrapie (H_s) agent (strain 263K) was prepared by homogenisation of infected brain tissue in phosphate buffered saline. The titre of the agent produced in this way is normally of the order of 10^7 - 10^9 LD₅₀ units ml⁻¹ as assayed by the intracranial route in hamster. A stock of the hamster adapted scrapie strain agent (263K) is stored at or below -70°C.

A microsomal fraction derived from crude brain homogenate was used for all spiking experiments.

The microsomal fraction was prepared according to the method of Millson et al (Millson GC, Hunter GD and Kimberlin RH (1971); "An experimental examination of the scrapie agent in the cell membrane mixtures. The association of scrapie activity with membrane fractions", J. Comp Path. 81, 255-265). Crude brain homogenate prepared from 263K infected brains by Dounce homogenisation was pelleted at 10,000g for 7min to remove nuclei, unbroken cells and mitochondria. The microsomes remaining in the supernatant were then pelleted by centrifugation at 100,000g for 90min, followed by resuspension in PBS.

2) Calculation of results

Clearance (C) and reduction (R) factors were calculated based on the end point dilution for samples after analysis by Western blotting. The end point dilution is calculated based on the first dilution at which no

scrapie prion protein (PrP^{sc}) can be detected. The reciprocal of this dilution is then taken as the titre of agent, and thus all titres are expressed in arbitrary units. Based on the titre determined by end point dilution, the total amount of PrP^{sc} in the sample is calculated based on the volume of the sample and taking into account any correction factors which need to be applied. Clearance factors are calculated relative to the theoretical input spike. Reduction factors are calculated relative to the level of PrP^{sc} detected in the load sample.

Where no PrP^{sc} is detected at the highest concentration of sample tested, then the reciprocal of the dilution is taken as 1, and clearance and reduction factors are expressed with a \geq sign proceeding the logarithmic value.

3) Western Blot Assay for Scrapie Infectivity

The titre of the stock of 263K used in this study, as well as the titre present in all samples generated during the study was determined by a Western blot procedure. This procedure relies upon the difference in susceptibility of the infectious (PrP^{sc}) and non-infectious (PrP^c) to proteinase K digestion. Samples were treated with protease K to digest away any PrP^{sc}, and run on a SDS polyacrylamide gel followed by blotting onto nitrocellulose. Any PrP remaining after protease digestion, corresponding to PrP^{sc}, was then detected using a PrP specific antibody. The relative level of scrapie in the samples compared to the stock was determined by serial dilution to end point (the

point where no signal was detected) of all samples.

Further information is given in A. Bailey, "Strategies for the Validation of Biopharmaceutical Processes for the Removal of TSE's", Cambridge Healthtech Institute, Nov.1998, Lisbon, Portugal.

Table 1 shows the efficiency of removal of spiked hamster scrapie prion proteins (PrP^{sc}) by various depth filters. Removal is expressed as clearance factor C (innoculum concentration/filtrate concentration) or as reduction factor R (feedstock concentration/filtrate concentration). The Seitz KS80 filter of pore size 0.6 to 1.5 microns according to the present invention is highly effective in removing the prion proteins. Other filters presented for comparison purposes having either a larger pore size or including cationic species are less effective.

EXAMPLES

Example 1 (Treatment of Albumin according to the invention)

A model system was set up to replicate on an experimental scale the depth filtration of albumin in the conventional plasma fractionation process, employing different types of filter. The albumin-containing sample (fraction V) was spiked with hamster scrapie prion protein produced as described above and the concentration thereof was assessed by Western Blotting also as described herein.

The filter was a Seitz KS80 (trademark) pad cut to a 142mm diameter disk of effective filtration area 128cm². The filter was pretreated by passing ethanol and NaCl

through for 35 minutes. The sample material was approximately 1 litre of resuspended fraction V at pH6.9 and 85.0g/l concentration taken from the conventional plasma fractionation process and kept at +4°C.

The conventional process involves the batch filtration of 853ml of sample. In this experiment, the same total volume of sample was passed through the filter, but only the final 100ml was spiked with microsomal hamster scrapie. 100ml of the sample starting material was spiked with 9.5ml of the preparation of microsomal hamster (263k) scrapie and a sample of the spiked material was removed for analysis of the level of PrP^{sc}. The spiked material was passed through the filter at a flow rate of 6.4ml/min and the filtrate collected for analysis of the level of PrP^{sc}. All samples were stored at or below -70°C until analysis of the level of PrP^{sc} was carried out. Before the samples were analysed by Western Blotting, any scrapie in the sample was concentrated by ultracentrifugation.

Table 1 shows that the removal assessed by clearance factor C and reduction factor R exceeds four log units. The filter is therefore most effective in removing the added spike of hamster scrapie prion protein.

Example 2 (Albumin Treatment - Comparison)

The fraction V albumin-containing sample was filtered with a different filter in a similar manner to Example 1.

The filter used was a Cuno (trademark) Delipid Del 1 mini cartridge of effective filtration area 27cm². The

filter was pretreated with ethanol and NaCl.

The sample material was fraction V at pH 6.9 and 85g/l concentration taken after conventional filtration through a Seitz KS80 filter and held at +4°C.

In this case, only the final 50ml were spiked with microsomal hamster scrapie. The spiked material was passed through the filter at a flow rate of 3.2ml/min and the filtrate analysed for prion protein as before. The extent of clearance is shown in Figure 2 but is only about two logs. The value R is experimental artefact and should be ignored.

Example 3 (IGG - Comparison)

The procedure of Example 1 was repeated on IgG-containing supernatant I and III from conventional plasma fractionation.

The filter was a Millipore lifeguard CP20 disk 47mm in diameter providing an effective filtration area of 12.5cm². The sample material was about 800ml of supernatant I and III (prefiltration) from the conventional plasma fractionation procedure and held at +4°C. It contained about 12% ethanol and had a pH 5.1.

680ml of sample was treated and the final 50ml was spiked with microsomal hamster scrapie.

The extent of removal of prion proteins is given in Table 1. The clearance factor C was three logs. The value R should be ignored and may involve experimental artifact.

Example 4 (IGG - Comparison

The general procedure of Example 1 was repeated on IgG-containing fraction II suspension from conventional plasma fractionation.

The filter was a Seitz K200 (trademark) of 1422mm diameter and effective filtration area 128cm². The sample material was resuspended fraction II from conventional plasma fractionation held at +4°C.

600ml of sample was passed through the filter and the final 100ml was spiked with microsomal hamster scrapie. The extent of removal of the PrP^{sc} was determined as before and the results are given in Table 1. It can be seen that removal was achieved to about 2 logs.

Thus, it can be seen from the Examples that greater than 10⁴ times removal of abnormal infective prion proteins (limit of detection) can be achieved using a neutral filter having a pore size of less than 2 microns.

13

TABLE 1**REMOVAL OF PRP^{sc} BY DEPTH FILTRATION**

FILTER (PRODUCT)	COMPOSITION	RETENTION (μm)	C	R
Seitz, KS80 (Albumin)	Cellulose, Kieselguhr Perlite	0.6 - 1.5	≥ 4.1	≥ 4.9
Seitz, K200P (IgG)	Cellulose, Kieselguhr Perlite	3.5 - 6.0	2.8	2.0
Cuno, Delipid 1 (Albumin)	Cellulose, Kieselguhr Cation Resin	0.6	2.8	<1
Millipore CP20 (IgG)	Borosilicate glass	2.0	3.0	<1

CLAIMS

1. A method for the removal of abnormal infective prion proteins associated with transmissible spongiform encephalopathies (TSEs) from an aqueous liquid containing a protein (especially a biologically active protein), which comprises passing the liquid through a depth filter formed of a matrix comprising solid particles of porous material having a pore size less than $2\mu\text{m}$.